

WO 00/09625

- 1 -

PCT/GB99/02623

5

10

15

10

20

25

30

35

40

45

50

55

Shale-Stabilizing Additives

This invention concerns drilling or completion fluids, particularly water-based drilling or completion fluids. More specifically, it pertains to additives for such fluids. Even more specifically, the invention relates to additives used to prevent shales or clayey formations from adversely affecting well drilling or well completion operations.

BACKGROUND OF THE INVENTION

Drilling fluids are used in well drilling operations, e.g., during drilling of oil and gas wells. During drilling, drilling fluid is pumped down a drillstring, discharged through ports in the drill bit and returned to the surface via the annulus between the drillpipe and the surrounding formation. The drilling fluid performs a variety of functions including cooling and lubricating the drill bit and drillstring, removing rock cuttings generated during the drilling process and carrying them to the surface, suspending cuttings in the annulus when pumping stops, preventing squeezing in or caving of the formation and keeping formation fluids at bay.

Drilling fluids generally comprise a carrier, a weighting agent and chemical additives. Drilling fluids fall into two main categories: water-based drilling fluids, also known as water based muds (WBMs), in which the carrier is an aqueous medium; and oil-based drilling fluids, also known as oil-based muds (OBMs), in which the carrier is oil or a water/oil emulsion. Oil based muds are technically superior to WBMs in certain important respects, including the comparative lack of adverse reactivity of OBMs with shales, one of the most commonly encountered rock types during drilling for oil and gas. The use of OBMs, however, has the disadvantage of resulting in production of large quantities of oil-contaminated waste products such as cuttings that are difficult to dispose of in an environmentally

5 acceptable way. While the use of WBMs is environmentally more
acceptable than of OBMs, the performance of WBMs, particularly
10 when drilling through water sensitive rocks such as shales, is
technically inferior to that of OBM. Shales exhibit great
5 affinity for water, and adsorption of water by shales causes the
shale to swell and produces chemical changes in the rock which
15 produce stresses that weaken the formation, possibly leading to
erosion of the borehole or loss of structure. This can lead to
drilling problems such as wellbore erosion or stuck pipe. In
10 addition, inferior wellbore quality may hinder logging and
completion operations.

20 Much effort has been put into improving the performance of WBM
relative to shales, namely improving the level of so called
15 shale inhibition of WBM. Various chemical additives have been
incorporated in WBM in attempts to improve shale inhibition. In
25 particular water soluble glycols, polyhydric alcohols (i.e.
chemicals containing more than one hydroxyl group) or
polyglycols (i.e. chemicals made using alkylene oxides such as
30 ethylene oxide or propylene oxide) are widely used for this
purpose, typically being added to WBM in amounts in the range 3
to 10% by weight. These chemicals can be collectively referred
to as Polyols. Polyols used in this way include, for example,
35 glycerols, polyglycerols, glycols, polyalkylene glycols (PAG),
eg polyethylene glycols (PEG), polypropylene glycols (PPG) and
25 copolymers of ethylene and propylene glycols, alcohol
ethoxylates (AET) and glycol ethers. A typical inhibitive AET is
40 an n-butanol derivative of ethylene oxide. The PAGs can have a
range of ethylene oxide: propylene oxide (EO:PO) ratios and can
30 be random or block copolymers; a frequently used material of
this type is understood to be a random copolymer with an EO:PO
45 ratio of about 1:1.

50 Variants of polyalkylene glycols and alcohol alkoxylates are for
example described in the International Patent Applications
WO-96/24645 and WO-96/24646. Others are found in the European
Patent Application EP-A-0495579, the United States Patents

US-A-4830765 and US-A-4172800.

A further source relating to the background of the invention is the Society of Petroleum Engineers Reports SPE 28960 (Mechanism of Shale Inhibition by Polyols in Water Based Drilling Fluids) proposing a credible mechanism that adequately describes how such polyols provide shale inhibition.

Copolymers of styrene and maleic anhydride and a number of derivatives are described for example in the United States Patent No. 3,332,872, for use as viscosity control agents. Hydrophilic-hydrophobic graft copolymers with polystyrene side chains for drilling fluids appear in the United States Patent No. 4,085,168. Other hydrophobically modified polymers based on polyacrylamide and hydroxyethylcellulose have been disclosed for example in the United States Patent Nos. 5,597,783 and 5,637,556.

Shale swelling is considered as a problem not only in the oil field industry. It is encountered as clay swelling in the mining industry, where this phenomenon causes severe difficulties when dewatering the mineral tailings.

In view of the above, it is an object of the invention to provide a novel additive for inhibiting shale swelling. It is another, more specific object of the invention to provide an additive for a WBM.

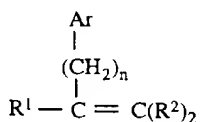
SUMMARY OF THE INVENTION

The objects of the invention are achieved by shale-stabilizing additives as set forth in the appended independent claims. According to a first aspect of the invention, there is provided a shale-stabilizing additive comprising a polymer based on an olefinically unsaturated hydrocarbon with alkylene oxide based side chains.

Useful olefinically unsaturated hydrocarbons generally are aliphatic olefinically unsaturated hydrocarbons or vinylidene aromatic monomers.

Aliphatic olefinically unsaturated hydrocarbons include, for example, α -olefin monomers containing from 2 to 28, preferably from 4 to 20, more preferably from 8 to 18 carbon atoms.

Preferred olefinically unsaturated hydrocarbons are vinylidene aromatic monomers. Suitable vinylidene aromatic monomers include, for example, those represented by the following formula:



wherein R^1 is hydrogen or an alkyl group containing 1 to 4 carbon atoms, preferably hydrogen or methyl; each R^2 is independently hydrogen or an alkyl group containing 1 to 4 carbon atoms, preferably hydrogen or methyl; Ar is a phenyl group or a phenyl group substituted with 1 to 5 C_1 - C_4 -alkyl substituents; and n has a value from zero to 4, preferably from zero to 2, most preferably zero. Preferred monomers are styrene or styrene derivatives including α -methyl styrene, the C_1 - C_4 -alkyl- or phenyl-ring substituted derivatives of styrene, such as ortho-, meta-, and para-methylstyrene, para-vinyl toluene or mixtures thereof. The most preferred vinylidene aromatic monomer is styrene.

The polymer is preferably a copolymer of an above-described olefinically unsaturated hydrocarbon and an ethylenically unsaturated carboxylic acid, carboxylic acid salt or carboxylic acid anhydride with alkylene oxide based side chains. Preferred olefinically unsaturated carboxylic acids contain 2 to 12, more preferably 2 to 6, carbon atoms in addition to the carboxyl group(s). They are preferably monocarboxylic acids or,

5

10

more preferably, dicarboxylic acids. Preferred examples thereof are acrylic acid, methacrylic acid, fumaric acid, maleic acid, the salts thereof, or maleic anhydride. Most preferably, maleic acid, maleic anhydride and/or a maleic acid salt is incorporated in the polymer. The alkali metal salts, particularly the sodium salt, are the preferred carboxylic acid salts.

15

20

25

30

35

40

45

50

55

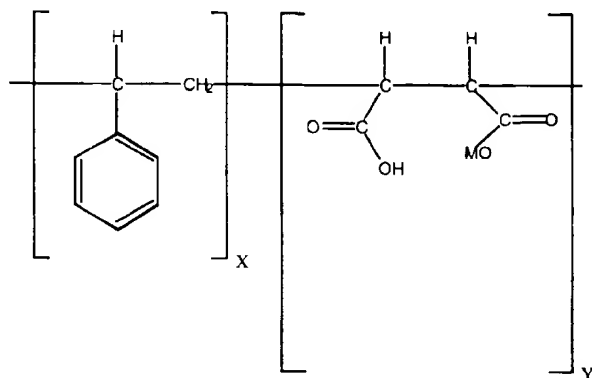
Alkylene oxide based side chains can be introduced into the polymer by esterification of carboxylic groups or anhydride groups with a polyoxyalkylated compound, such as a polyoxyalkylated alcohol. The esterification step can be carried out before or after the polymerization reaction of the dicarboxylic acid (salt) or the anhydride with the vinylidene aromatic monomer. The polymerization reaction and the esterification step are generally known in the art. Preferably 2 to 75 percent, more preferably 20 to 60 percent, most preferably about 50 percent of the total number of carboxyl carbon atoms in the polymer are esterified.

In a preferred embodiment of the invention, the polymer is a copolymer of styrene or a styrene derivative and maleic anhydride with alkylene oxide based side chains.

The molecular weight of the additive is preferably from 5000 g/mol to 100,000 g/mol, more preferably from 10,000 g/mol to 30,000 g/mol. The preferred weight of the alkylene oxide based side chain in accordance with the invention is above 200 g/mol and below 1500 g/mol, more preferably 300-600 g/mol.

The number of alkoxylate groups, e.g. $-\text{CH}_2-\text{CHR}-\text{O}-$ with R being H, CH_3 , or CH_2-CH_3 , per side chain is preferably up to 60 units.

A preferred molecule in accordance with the invention has the molecular structure:



M in each occurrence independently is hydrogen or $-(CH_2-CHR-O-)_n-CH_3$ with R being CH_3 or CH_2-CH_3 or, preferably, hydrogen, with the proviso that at least some of the radicals M have the meaning of $-(CH_2-CHR-O-)_n-CH_3$. X and Y each independently are from 1 to 100. The total of X and Y should generally be greater than 4 and the invention works best if the total of X and Y is greater than 50. The ratio of X : Y is preferably from 1 : 3 to 3 : 1, more preferably about 1 : 1. The value of n is from 3 to 70, preferably greater than 4 and less than 60. More preferably, n is 7-25.

The above-described polymer is preferably used as an additive in water-based drilling fluids (WBM) or completion fluids or in dewatering operations for mineral tailings.

In another aspect, the invention concerns a drilling fluid with 0.1 to 10 weight per cent (wt%) of the polymer as characterized before. More preferably, the polymer are used at 2 to 7 wt%.

The additives in accordance with the invention provide higher levels of shale swelling inhibition in the presence of weakly hydrated cations, such as potassium, cesium, and ammonium. Inhibition can be obtained solely from using the additives in freshwater or preferably in combination with salts containing for example sodium, calcium, magnesium, or potassium ions.

It can also be expected that the novel additives can improve current methods of dewatering mineral tailings in the mining industry, as today this process is severely hampered by clay swelling.

These and other features of the invention, preferred embodiments and variants thereof, and further advantages of the invention will become appreciated and understood by those skilled in the art from the detailed description following below.

EXAMPLE(S) FOR CARRYING OUT THE INVENTION

The preparation of the chemicals compounds used in the following examples as additives is known. Following the preparation steps laid out for example by H. Dérand et al. in *Macromolecules* 29 (1996), 8770-8775 and by A. Eckert and S.E. Weber in *Macromolecules* 29 (1996), 560-567, copolymers of styrene and maleic acid (SMACs) can be grafted with poly(ethylene glycol) (PEGs) or derivatives, thereof.

The shale inhibition capabilities of additives can be assessed by a number of laboratory techniques such as cuttings dispersion, cuttings hardness and shale swelling tests. These tests are suitable for rapid screening of new additives and are widely used in the industry.

Shale recovery from bottle rolling tests have been used to measure the shale inhibition properties. Tests were done using Oxford Clay cuttings (a water sensitive shale) sieved to 2 - 4 mm. Briefly, the test is a modification of a standard oilfield cuttings dispersion test and consists of adding 10 g of test substrate (Oxford Clay) with 100 ml of test fluid in a 300 ml bottle. The test samples are rolled at 50 rpm for 4 hours. This encourages breakdown and dispersion of the cuttings if they become soft due to interaction with the test fluid. The shale

cuttings are sieved through a 250 micron screen and the amount of shale recovered is measured after drying in an oven. The poly(ethylene glycol) (PEG) used in these tests had a molecular weight of about 600 g/mol.

Bottle rolling tests were done with 5 % w/v solutions of the invention in 7.6 % (Table 1) and 12.9 % w/w KCl (Table 2). The grafted copolymer used in both of these cases was the same. The backbone consisted of an alternating copolymer of styrene and maleic anhydride (SMAC) with grafted poly(ethylene glycol) monomethyl ethers (MPEG 500) side chains of about 500 g/mol. A significant increase in the amount of shale recovered was observed when the invention was used over that of PEG / KCl. A comparison of the results of Table 1 and 2 shows that the amount of shale recovered by the invention increased with the amount of KCl.

TABLE 1. Shale recovery results from bottle rolling tests with Oxford clay cuttings for polyglycol and SMAC grafted copolymer in 7.6 % w/w KCl.

Sample	% Shale Recovery
7.6 % KCl	20
PEG	39
SMAC (MPEG 500)	64

TABLE 2. Shale recovery results from bottle rolling tests with Oxford clay cuttings for PEG and SMAC copolymer with MPEG 500 grafts in 12.9 % w/w KCl.

Sample	% Shale Recovery
12.9 % KCl	29
PEG	51
SMAC (MPEG 500)	91

The amount of shale recovery of the invention as a function of the grafted MPEG chain length is shown in Table 3. The results show that all MPEG variations of the invention show improved shale recovery compared to that of polyethylene oxide and that the best results are obtained for copolymers with MPEG grafts with molecular weight of about 300 to 400 g/mol.

TABLE 3. Shale recovery results from bottle rolling tests with Oxford clay cuttings for polyglycol and grafted copolymer in 7.6 % w/w KCl where the molecular weight of graft polyethylene oxide varies from 200 to 1500 g/mol.

Sample	% Shale Recovery
-----	-----
15 7.6 % KCl only	25
25 PEG	38
SMAC MPEG 200	54
SMAC MPEG 300	87
SMAC MPEG 400	85
20 SMAC MPEG 500	72
SMAC MPEG 600	69
SMAC MPEG 750	70
SMAC MPEG 1100	66
SMAC MPEG 1500	49

Table 4 shows bottle rolling test results in 12.9 % w/w KCl that include a polymer that consists of a backbone with 2 styrene units for every maleic anhydride unit. MPEG 500 was used as the grafting polymer. The results show that increasing the amount of styrene in the backbone increased the amount of shale recovered.

TABLE 4. Shale recovery results from bottle rolling tests with Oxford clay cuttings for polyglycol and grafted copolymer in 12.9 % w/w KCl. The backbone of SMAC 2:1 Styrene MPEG 500 was composed of 2 styrene units for every maleic anhydride. The grafts consisted of MPEG 500.

Sample	% Shale Recovery
-----	-----

12.9 % KCl	27
PEG	53
SMAC MPEG 500	85
SMAC 2:1 Styrene MPEG 500	95

The effect of drilling fluid additives on reactive shales can also be assessed by the Hassler Cell test. Briefly, fluids are pumped through a confined Oxford Clay core perpendicular to the bedding planes at high pressure and the permeability of the core to the test fluid is measured and compared with that of a synthetic pore fluid. In general, greater shale inhibition can be achieved by reducing the permeability of the test fluid within the core. For instance, the permeability of oil based muds (OBM) is much lower than the pore fluid due, in part, to the change in wettability caused by OBM surfactants. Inhibitive water based drilling fluids also show significant reductions in fluid permeability. PEG / KCl based fluids show permeability reductions from 11 to 46 % and silicate based systems show reductions of between 65 - 80 %. The permeability reduction caused by the invention (SMAC MPEG 500) was about 96.9 %. This is the greatest amount of reduction for a water based fluid observed to date and is equal to that of an oil based drilling fluid.

TABLE 5. Flow Rate Changes in Oxford Clay Cores by Various Fluids in Hassler Cell Tests.

Fluid type	Flow Rate before [g/hr]	Flow Rate after [g/hr]	% Original Rate
-----	-----	-----	-----
10 % KCl	0.043	0.061	142
PEG / KCl	0.037	0.033	89
PEG-C ₆ H ₆ / KCl	0.037	0.020	54
KCl / Silicate	0.052	0.010	19
NaCl then			
KCl / Silicate	0.068	0.024	35
70:30 OBM	0.036	0.0024	6.6

SMAC(MPEG 500)/KCl 0.1397 0.0043 3.1

Improved shale inhibition is exhibited by many variations of the invention as is shown above. The improved shale inhibition is primarily the result of the hydrophobic portions of the molecule and inhibition increases with the amount of styrene in the backbone. The invention appears to provide shale inhibition by reducing the permeability of aqueous solutions in reactive shales.

The invention also shows improved results in bulk cuttings hardness test which is a modification of a standard industry analysis. In this experiment 30 g of sieved Oxford Clay cuttings (2-4 mm) were put in 200 mls of the test fluid for 2 hours. The test fluid is drained off and the cuttings are put into a press cell. The cuttings are then pressed through a plate with holes and the amount of torque required is measured with every turn of the torque gauge. The plateau torque is quoted as the cuttings hardness. Table 6 shows the results of tests conducted on a series of test samples in 12.9 % KCl. PEG and SMAC MPEG 500 samples contained 5 % w/v test additive.

TABLE 6. Bulk Cuttings hardness in 12.9 % KCl fluids.

Sample	Cuttings Hardness [N*m]
-----	-----
12.9 % KCl	1.6
PEG	8
SMAC MPEG 500	12
natural Oxford Clay (no fluid)	14

The results in Table 6 show that the MPEG grafted copolymers results in harder cuttings than the polyethylene glycol / KCl mud.

The results of clay dispersion, Hassler Cell and cuttings hardness tests clearly show the improved levels of inhibition

provided by fluids containing MPEG grafted SMAC copolymer in place of poly(alkylene oxides) in KCl based fluids.

The performance of the KCl / SMAC system was measured as a function of the KCl concentration, SMAC concentration and fluid conditions. The performance was found to increase with the concentration of KCl and SMAC up to a threshold value after which performance levelled. Tests conducted with Oxford clay found that the threshold concentration of KCl to be between 10 and 14 % w/w. The threshold value for maximum performance of SMAC was between 1 and 2 % w/v.

SMAC performance increased substantially if residual maleic anhydride groups present were hydrolysed to the acid form. SMAC with maleic acid groups are sensitive to the pH of the fluid. The optimum shale recovery was found to occur at pH of 9. Excellent performance was observed for SMAC fluids in the pH range of 7 to 11. Shale inhibition declined rapidly above pH of 11.5

Replacement of the polyethylene glycol side chains with polypropylene glycol based side chains gave inferior results.